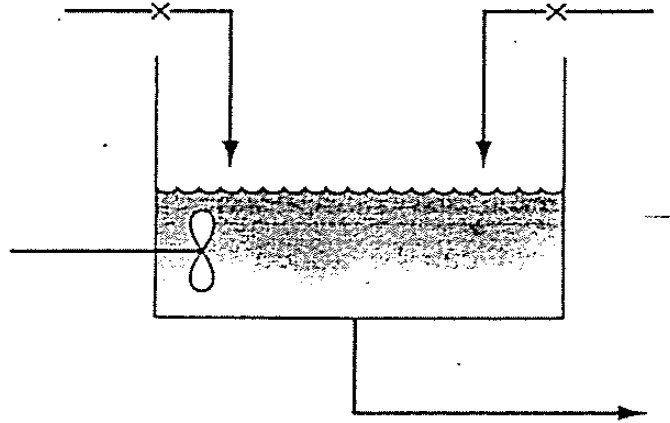
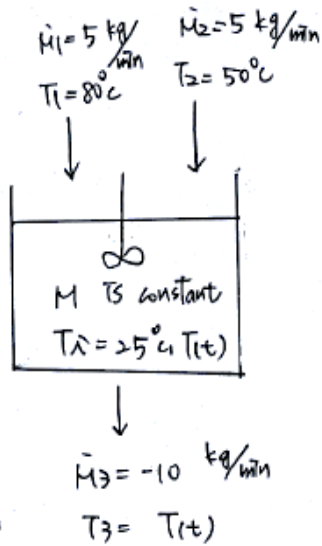


3.13 The mixing tank shown here initially contains 50 kg of water at 25°C. Suddenly the two inlet valves and the single outlet valve are opened, so that two water streams, each with a flow rate of 5 kg/min, flow into the tank, and a single exit stream with a flow rate of 10 kg/min leaves the tank. The temperature of one inlet stream is 80°C, and that of the other is 50°C. The tank is well mixed, so that the temperature of the outlet stream is always the same as the temperature of the water in the tank.

- Compute the steady-state temperature that will finally be obtained in the tank.
- Develop an expression for the temperature of the fluid in the tank at any time.



3.13



(a) <sol> Take tank as the system (open steady-state system)

$$\frac{dU}{dt} = \dot{M}_1 \hat{H}_1 + \dot{M}_2 \hat{H}_2 + \dot{M}_3 \hat{H}_3 + \overset{\text{no heat}}{Q} + \overset{\text{no shaft work}}{W} + \overset{\text{no P work}}{P}$$

$$\Rightarrow 5 \hat{H}_1 + 5 \hat{H}_2 - 10 \hat{H}_3 = 0$$

$\frac{\text{kg}}{\text{min}} \quad \frac{\text{kg}}{\text{min}} \quad \frac{\text{kg}}{\text{min}}$

$$\hat{H}(T) = \hat{H}(T_R) + \int_{T_R}^T C_p(T) dT, \text{ assume } C_p \text{ is not a function of temp.}$$

\downarrow
 reference temp

$$= \hat{H}(T_R) + C_p(T - T_R)$$

$$\Rightarrow 5 \hat{H}(T_R) + 5 C_p (80 - T_R) + 5 \hat{H}(T_R) + 5 C_p (50 - T_R) - 10 \hat{H}(T_R) - 10 C_p (T_3 - T_R) = 0$$

$$\Rightarrow T_3 = 65^\circ\text{C}$$

(b) Open Unsteady-state system

$$\frac{d(\hat{U})^{\text{system}}}{dt} = \dot{M}_1 \hat{H}_1 + \dot{M}_2 \hat{H}_2 + \dot{M}_3 \hat{H}_3 + \dot{Q} + \dot{W}$$

$$\frac{d(M\hat{U})}{dt} = M \frac{d(\hat{U})}{dt} = M C_v \frac{dT}{dt}$$

$$\Rightarrow 50 C_v \frac{dT_3}{dt} = 5 \hat{H}(T_R) + 5 C_p (80 - T_R) + 5 \hat{H}(T_R) + 5 C_p (50 - T_R) - 10 \hat{H}(T_R) - 10 C_p (T_3 - T_R)$$

$$\Rightarrow 50 C_v \frac{dT_3}{dt} = 5 C_p (130) - 10 C_p T_3$$

for liquid & solid: $\hat{H} = \hat{U} + P\hat{V}$
 $\Rightarrow d\hat{H} = d\hat{U} + P d\hat{V} + \hat{V} dP$
 \hat{V} is small for liq. & solid
 \hat{V} remain constant for liq. & solid

$$\Rightarrow C_p dT \approx C_v dT$$

$$\Rightarrow C_p \approx C_v$$

$$\Rightarrow 10 \frac{dT_3}{dt} = 130 - 2T_3$$

$$\Rightarrow \frac{dT_3}{dt} + \frac{1}{5} T_3 = 13$$

$$\Rightarrow T_3 = C_1 \cdot e^{-\frac{1}{5}t} + C_2$$

$$\text{at } t=0, \quad T_3 = 25^\circ\text{C}$$

$$\text{at } t \rightarrow \infty, \quad T_3 = 65^\circ\text{C}$$

$$\Rightarrow \begin{cases} 25 = C_1 + C_2 \\ 65 = 0 + C_2 \end{cases} \Rightarrow C_1 = -40$$

$$\Rightarrow T_3 = -40^\circ\text{C} \cdot e^{-\frac{t}{\tau}} + 65^\circ\text{C}$$